Ch. 4 Mathematical Modeling of Fluid Systems and Thermal Systems

4-4 Hydraulic systems

operating pressure; 1~35 MPa, 70Mpa combination of electrical and hydraulic systems

* Hydraulic Servo System

Fig.4.17 Hydraulic servo motor

Linearization of a hydraulic servo system

$$A_1 = A_3 = k(\frac{x_0}{2} + x)$$

$$A_2=A_4=k(\frac{x_0}{2}-x)$$

k: constant, γ : specific weight

$$\begin{split} q_1 &= c_1 A_1 \sqrt{\frac{2g}{\gamma}(P_s - P_1)} = C_1 \sqrt{P_s - P_1} \left(\frac{x_0}{2} + x\right) \\ q_2 &= c_2 A_2 \sqrt{\frac{2g}{\gamma}(P_s - P_2)} = C_2 \sqrt{P_s - P_2} \left(\frac{x_0}{2} - x\right) \\ q_3 &= c_1 A_3 \sqrt{\frac{2g}{\gamma}(P_2 - P_o)} = C_1 \sqrt{P_2 - P_o} \left(\frac{x_0}{2} + x\right) = C_1 \sqrt{P_2} \left(\frac{x_0}{2} + x\right) \\ q_4 &= c_2 A_4 \sqrt{\frac{2g}{\gamma}(P_1 - P_o)} = C_2 \sqrt{P_1 - P_o} \left(\frac{x_0}{2} - x\right) = C_2 \sqrt{P_1} \left(\frac{x_0}{2} - x\right) \end{split}$$

$$q = q_1 - q_4 = C_1 \sqrt{P_s - P_1} \left(\frac{x_0}{2} + x \right) - C_2 \sqrt{P_1} \left(\frac{x_0}{2} - x \right)$$

$$q = q_3 - q_2 = C_1 \sqrt{P_2} \left(\frac{x_0}{2} + x \right) - C_2 \sqrt{P_s - P_2} \left(\frac{x_0}{2} - x \right)$$

incompressible fluid, symmetrical

$$\begin{split} q_1 &= q_3 \,, \ q_2 = q_4 \\ P_s &= P_1 + P_2 \,, \ \Delta P \overset{\Delta}{=} P_1 - P_2 \\ P_1 &= \frac{P_s + \Delta P}{2} \,, \ P_2 = \frac{P_s - \Delta P}{2} \end{split}$$

$$\begin{split} q &= q_1 - q_4 = C_1 \sqrt{\frac{P_s - \Delta P}{2}} \left(\frac{x_0}{2} + x\right) - C_2 \sqrt{\frac{P_s + \Delta P}{2}} \left(\frac{x_0}{2} - x\right) & => f(x, \Delta P) \\ q &- \overline{q} = a(x - \overline{x}) + b(P - \Delta \overline{P}) \\ \overline{q} &= f\left(\overline{x}, \Delta \overline{P}\right) \end{split}$$

valve coefficients;

$$a = \frac{\partial f}{\partial x}|_{\overline{x}, \Delta \overline{p}}$$

$$= C_1 \sqrt{\frac{P_s - \Delta \overline{P}}{2}} + C_2 \sqrt{\frac{P_s + \Delta \overline{P}}{2}}$$

$$\begin{split} b &= \frac{\partial f}{\partial \Delta p}|_{\overline{x}, \Delta \overline{p}} \\ &= - \left[\frac{C_1}{2\sqrt{2}\sqrt{P_s - \Delta \overline{p}}} \left(\frac{x_o}{2} + \overline{x} \right) + \frac{C_2}{2\sqrt{2}\sqrt{P_s + \Delta \overline{p}}} \left(\frac{x_o}{2} - \overline{x} \right) \right] < 0 \end{split}$$

Normal operating point;

$$\overline{x} = 0$$
, $\Delta \overline{p} = 0$, $\overline{q} = 0$

Linearized mathematical model

$$q = K_{1}x - K_{2}\Delta P$$

$$= (C_{1} + C_{2})\sqrt{\frac{P_{s}}{2}}x - (C_{1} + C_{2})\frac{x_{0}}{4\sqrt{2}\sqrt{P_{s}}}\Delta P$$

$$q = A_{p}\rho\dot{y}$$

$$A_{p}\Delta p = m\ddot{y} + b\dot{y}$$
(4.27)

Fig.4.26

(1) temp of inflowing liquid: constant hi; small change in heat input rate

heat balance;

$$\begin{split} Cd\theta &= (h_i - h_o)dt \\ C\frac{d\theta}{dt} &= h_i - h_o \\ R &= \frac{\theta}{h_o} = \frac{1}{Gc} \end{split}$$

$$RC\frac{d\theta}{dt} + \theta = Rh_i \quad \Rightarrow \quad \frac{\Theta(s)}{H_i(s)} = \frac{R}{RCs + 1}$$

(2) temp of inflowing liquid is changed : $\theta(i)$ heat input rate H, liquid flow rate G (kg/s); constant heat output flow rate change ; ho

heat balance;

$$\begin{split} &Cd\theta = (Gc\theta\left(i\right) - h_o)dt \\ &RC\frac{d\theta}{dt} + \theta = \theta\left(i\right) \ = > \ \, \frac{\Theta\left(s\right)}{\Theta_i(s)} = \frac{1}{RCs + 1} \end{split}$$

(3) temp of inflowing liquid, heat input rate; change liquid flow rate; constant

$$RC\frac{d\theta}{dt} + \theta = \theta(i) + Rh_i$$